Amendments to the Claims:

The following listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims

1. (Currently Amended) A continuous process for simultaneously preparing ~~making~~ multiple grades of base oil products and middle distillates from a mineral crude derived feed, wherein said process comprises the following steps:

(a) hydrocracking a mineral crude derived feed, comprising a vacuum gas oil having more than 10 wt % compounds present therein boiling above 470 °C, utilizing a hydrocracking catalyst comprising an acidic large pore size zeolite within a porous support material with an added metal having a hydrogenation/dehydrogenation function, wherein said added metal is a Group VIII/Group VIB combination, to thereby provide a conversion level of between 15 and 90 wt% and obtaining an effluent;

(b) distilling the effluent as obtained in step (a) into at least one middle distillate product and a full range residue boiling substantially above 340 °C but without separating compounds boiling above 420°C from said full range residue;

(c) catalytically dewaxing the entire full range residue as obtained in step (b) by contacting the full range residue with a dewaxing catalyst comprising a dealuminated extrudate of a zeolite of the MTW type and a low acidity refractory binder material wherein the weight ratio of said zeolite to said low acidity refractory binder material is in the range of from 5:95 to 95:5 and a Group VIII metal of either platinum or palladium that is present in said dewaxing catalyst in the range of from 0.1 to 5.0% by weight, thereby obtaining a dewaxed oil;

(d) hydrofinishing at least part of ~~distilling~~ the dewaxed oil obtained in step (c) to provide a hydrofinished, dewaxed oil ~~into a gas oil fraction and a fraction boiling below the gas oil fraction, which is below 400 °C~~;

(e) distilling the hydrofinished, dewaxed oil ~~hydrofinishing the gas oil fraction~~ obtained in step (d) to simultaneously provide multiple grades of base oil products; and ~~a heavy base oil~~

(f) isolating a dewaxed gas oil from the dewaxed oil as obtained in step (c), wherein the dewaxed heavy gas oil obtained in step (c) comprises between 10 and 40 wt% of a dewaxed heavy gas oil boiling for more than 70 wt% between 370 and 400°C.

2. (Previously Presented) The process according to claim 1, wherein more than 20 wt% of the compounds present in the vacuum gas oil boils above 470 °C.

3. (Previously Presented) The process according to claim 2, wherein at least a portion of the fraction boiling below the gas oil fraction is recycled to step (b) to be mixed with the effluent before distilling thereof.

4. (Previously Presented) The process according to claim 3, wherein from 0 to 15 wt% of the full range residue as obtained in step (b) is recycled to step (a) to be mixed with the mineral crude derived feed before hydrocracking thereof.

5. (Previously Presented) The process according to claim 4, further comprising adding a Fischer-Tropsch derived partly isomerised paraffin fraction to the full range residue prior to catalytically dewaxing.

Claim 6 (Canceled).

7. (Currently Amended) The process according to claim 5, wherein the hydrogen partial pressure in step (c) is greater than 100 bars.

8. (Currently Amended) The process according to claim 1 ~~7~~, wherein the multiple grades of base oil products simultaneously ~~heavy base oil~~ obtained in step (e) comprises a spindle oil, a light machine oil and a medium machine oil ~~more than 95 wt% saturates and has a viscosity index of between 95 and 120~~.

Claims 9-11 (Canceled).

12. (Previously Presented) The process according to claim 1, wherein the zeolite content of the dewaxing catalyst is between 5 wt.% and 35 wt.%.

13. (Previously Presented) The process according to claim 12, wherein the low acidity refractory binder material is selected from silica, zirconia, titanium dioxide, germanium dioxide, boria, and mixtures of two or more thereof.

14. (Previously Presented) The process according to claim 13, wherein the zeolite of the dewaxing catalyst has an average crystal size smaller than 0.5 μm.

15. (Previously Presented) The process according to claim 14, wherein the dewaxing catalyst, prior to metals addition, has an alpha value below 50.

16. (Previously Presented) The process according to claim 15, wherein the low acidity refractory binder material is silica and is essentially free of alumina.

17. (Currently Amended) A continuous process for simultaneously preparing ~~making a~~ multiple grades of base oil products and middle distillates from a mineral crude derived feed, where said process comprises:

hydrocracking a mineral crude derived feed, comprising a vacuum gas oil having more than 10 wt% compounds present therein boiling above 470 °C, using a hydrocracking catalyst, comprising an acidic large pore zeolite, a porous support material, and added metal having a hydrogenation/dehydrogenation function, wherein said added metal is a Group VIII/Group VIB combination, to thereby provide a conversion level of between 15 and 90 wt% and obtaining a hydrocracker effluent;

distilling said hydrocracker effluent into a middle distillate product and a full range residue product having a property such that more than 80 wt % boils above 340 °C and wherein compounds boiling above 420°C are not separated from said full range residue product;

catalytically dewaxing said full range residue product by contacting said full range residue product with a dewaxing catalyst comprising a dealuminated extrudate of a zeolite of the MTW type and a low acidity refractory binder material, wherein said dealuminated extrudate has a weight ratio of said zeolite to said low acidity refractory binder material in the range of from 5:95 to 95:5, and a Group VIII metal of either platinum or palladium that is present in said dewaxing catalyst in the range of from 0.1 to 5.0 % by weight, to thereby obtain a dewaxed oil;

distilling the dewaxed oil obtained in step (c) to remove a gas oil fraction and a fraction boiling below the gas oil fraction, which is below 400 °C; ~~and~~

hydrofinishing the dewaxed oil from which the gas oil fraction and fraction boiling below the gas oil fraction has been removed to provide a dewaxed, hydrofinished ~~said base~~ oil ~~product;~~

distilling the hydrofinished, dewaxed oil to simultaneously provide multiple grades of base oil products; and

isolating a dewaxed gas oil from the dewaxed oil as obtained in step (c), wherein the dewaxed heavy gas oil obtained in step (c) comprises between 10 and 40 wt% of a dewaxed heavy gas oil boiling for more than 70 wt% between 370 and 400°C.

18. (Previously Presented) A process according to claim 17, wherein the zeolite content of the dewaxing catalyst is between 5 wt.% and 35 wt.%.

19. (Previously Presented) A process according to claim 18, wherein the low acidity refractory binder material is selected from silica, zirconia, titanium dioxide, germanium dioxide, boria, and mixtures of two or more thereof.

20. (Previously Presented) A process according to claim 19, wherein the zeolite of the dewaxing catalyst has an average crystal size smaller than 0.5 μm.

21. (Previously Presented) A process according to claim 20, wherein the dewaxing catalyst, prior to metals addition, has an alpha value below 50.

22. (Previously Presented) A process according to claim 21, wherein the low acidity refractory binder material is silica and is essentially free of alumina.

23. (Previously Presented) A process according to claim 22, wherein up to 15 wt % of said full range residue product is recycled to be mixed with said mineral crude derived feed.

24. (Currently Amended) A process according to claim 23, further comprising adding a Fischer-Tropsch derived partly isomerised paraffin fraction to the full range residue prior to catalytically dewaxing.